



US010018304B2

(12) **United States Patent**
Poorman

(10) **Patent No.:** **US 10,018,304 B2**

(45) **Date of Patent:** **Jul. 10, 2018**

(54) **CNG FUELING SYSTEM**

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(*) Notice: Subject to any disclaimer, the term of this patent is extended or adjusted under 35 U.S.C. 154(b) by 0 days.

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(21) Appl. No.: **15/709,084**

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(22) Filed: **Sep. 19, 2017**

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(65) **Prior Publication Data**

US 2018/0003344 A1 Jan. 4, 2018

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Related U.S. Application Data

(63) Continuation-in-part of application No. 13/756,092, filed on Jan. 31, 2013, now Pat. No. 9,765,930.

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(60) Provisional application No. 61/593,134, filed on Jan. 31, 2012.

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(51) **Int. Cl.**
F17C 5/06 (2006.01)

(57) **ABSTRACT**

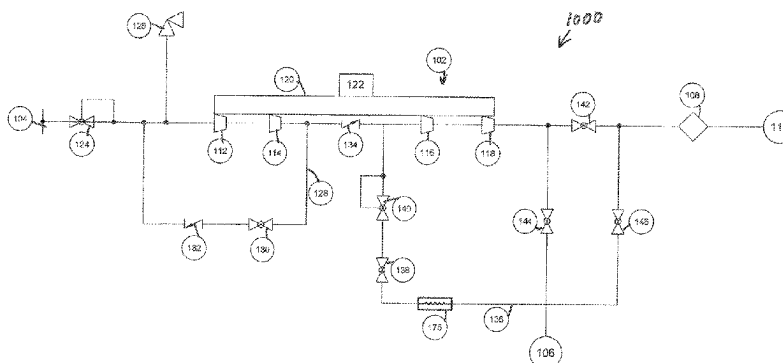
(52) **U.S. Cl.**
CPC **F17C 5/06** (2013.01); **F17C 2205/0338** (2013.01); **F17C 2221/033** (2013.01); **F17C 2227/0327** (2013.01); **F17C 2260/02** (2013.01); **F17C 2270/0168** (2013.01)

A compressed natural gas (CNG) fueling system has a single compressor comprising a first compression stage and a subsequent compression stage, wherein the first compression stage feeds the subsequent compression stage when filling a storage tank, the storage tank is configured to receive CNG from at least one of the first compression stage and the subsequent compression stage of the compressor when filling the storage tank, a CNG feedback to the subsequent compression stage of the compressor from the storage tank, the CNG being introduced back into the compressor at a location downstream relative to an output of the first compression stage, and a first heat exchanger associated with the CNG feedback.

(58) **Field of Classification Search**
CPC F17C 5/06; F17C 2270/0168; F17C 2260/02; F17C 2205/0338; F17C 2221/033; F17C 2227/0327; F17C 2223/0123; F17C 2265/065

See application file for complete search history.

15 Claims, 15 Drawing Sheets



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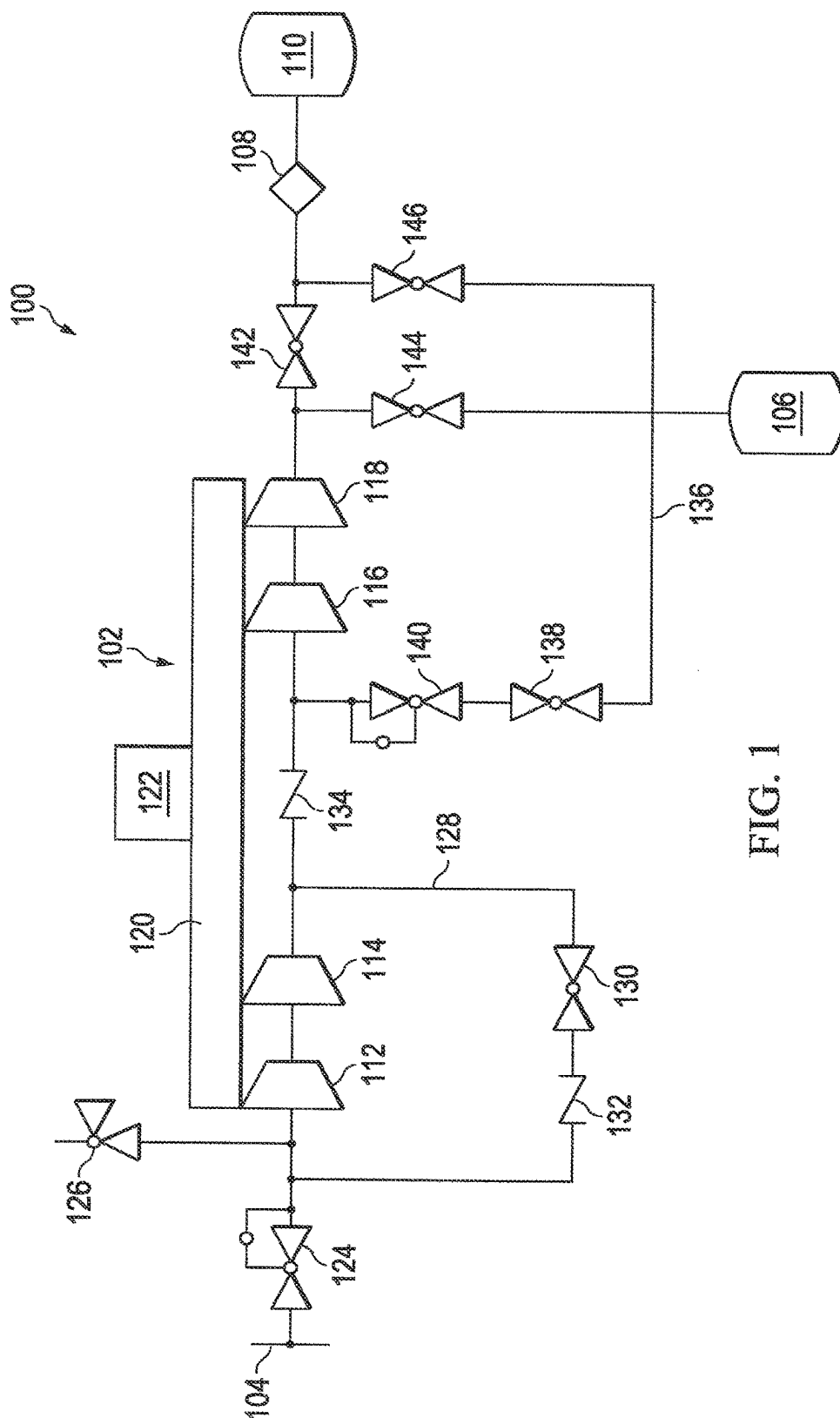


FIG. 1

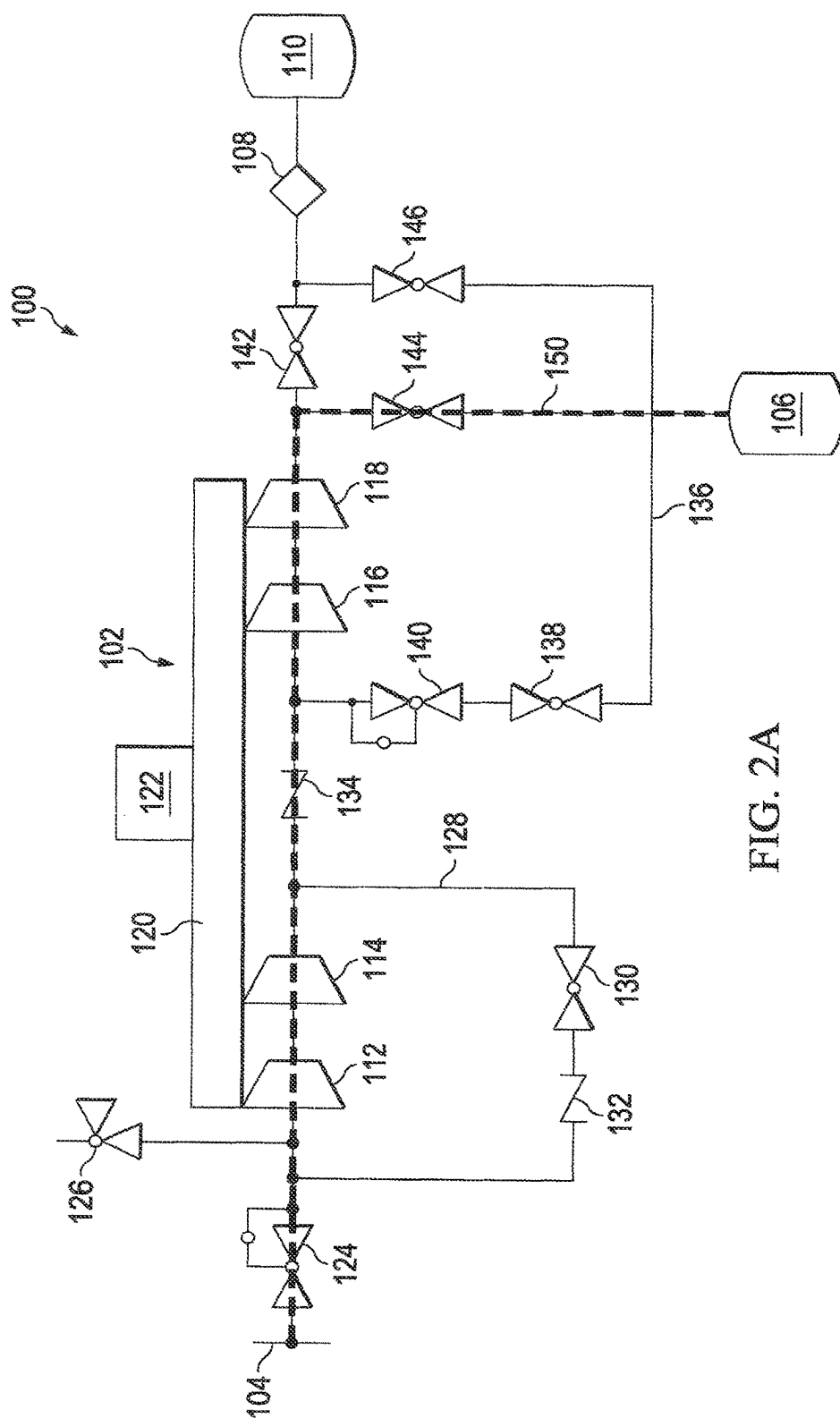


FIG. 2A

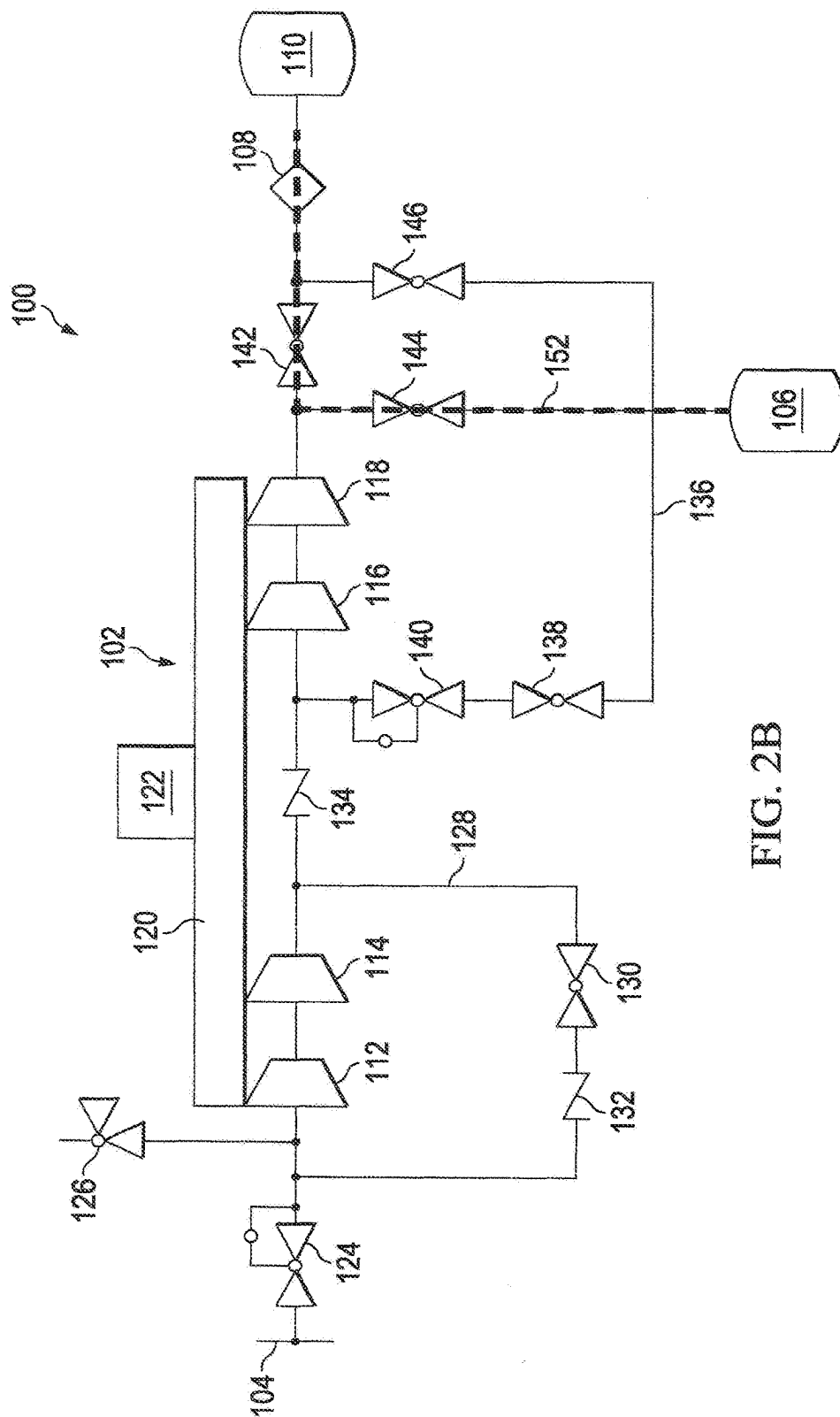


FIG. 2B

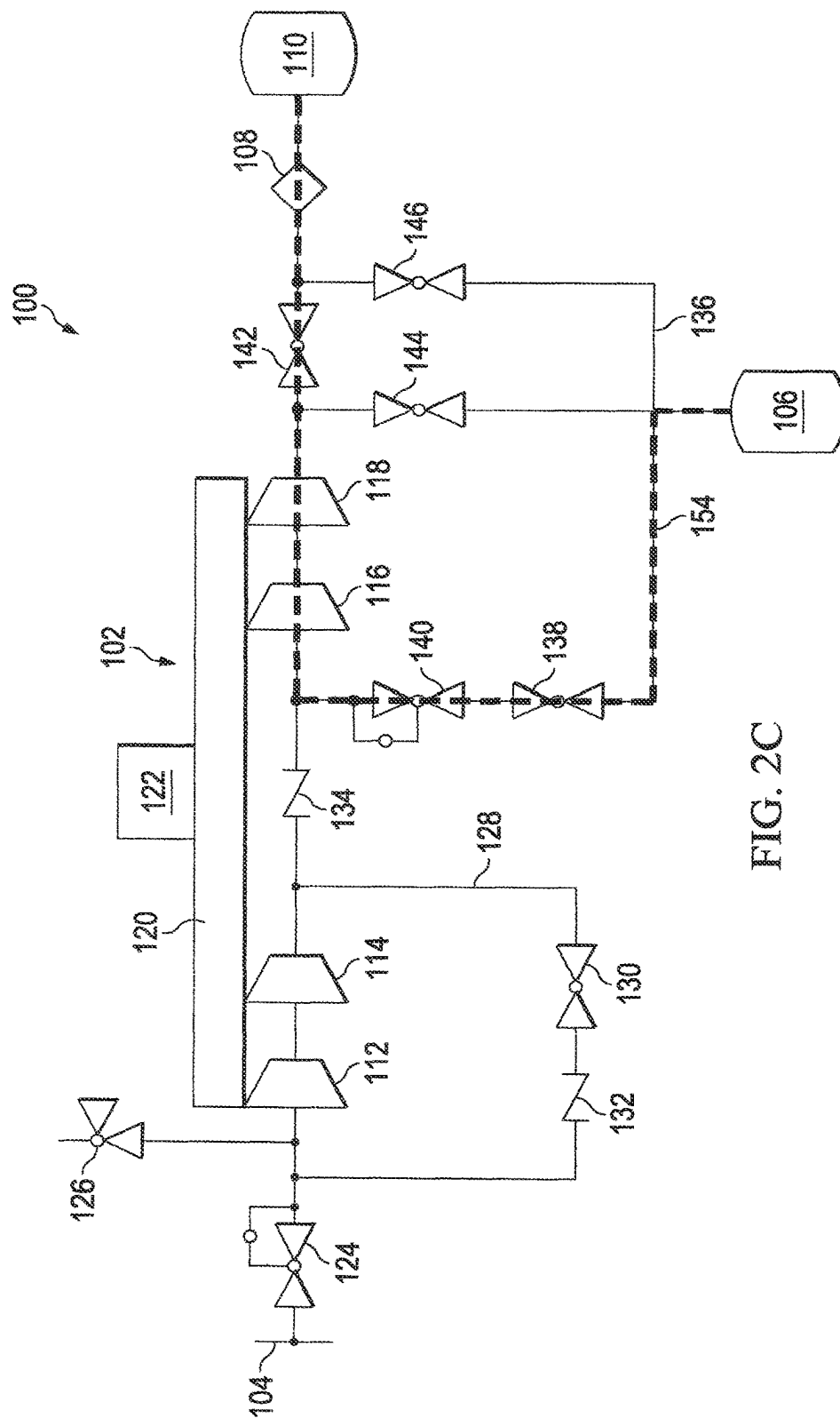


FIG. 2C

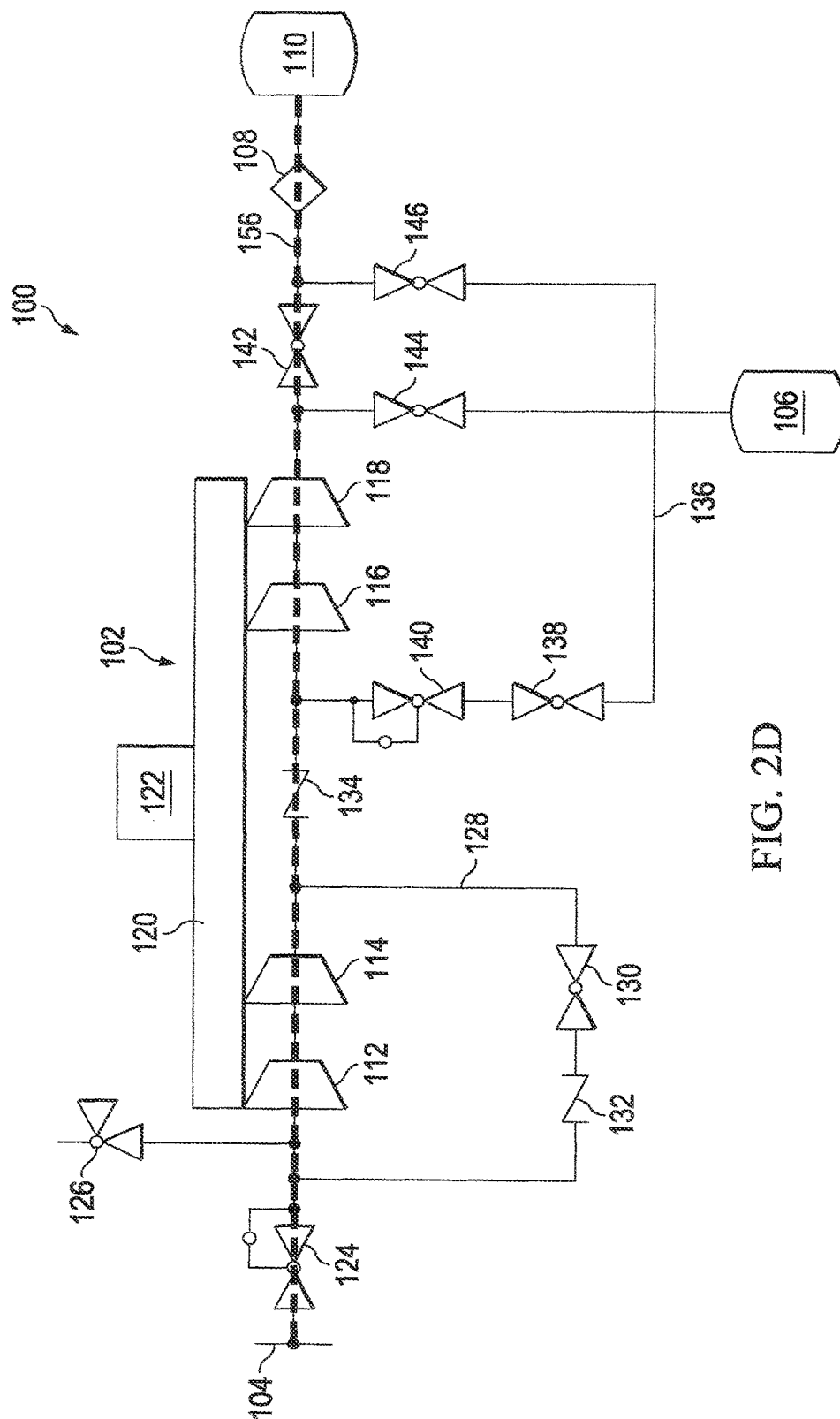
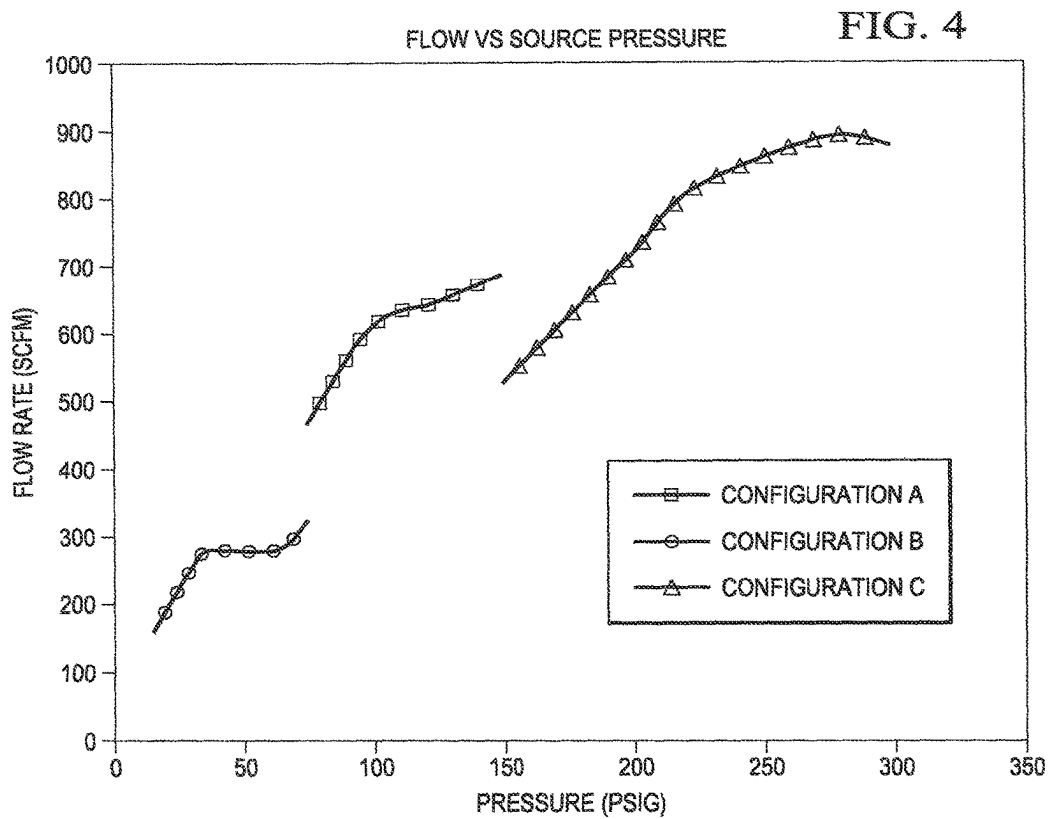
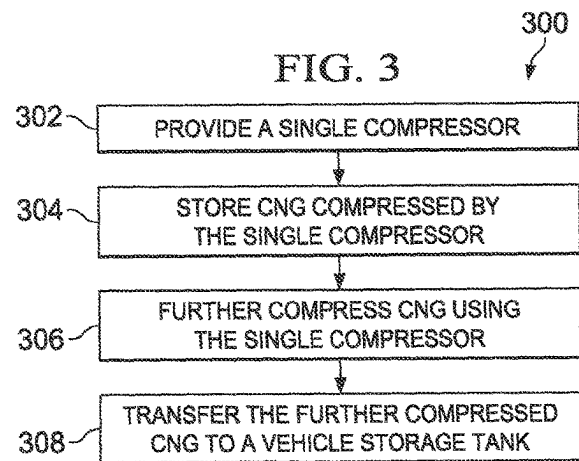
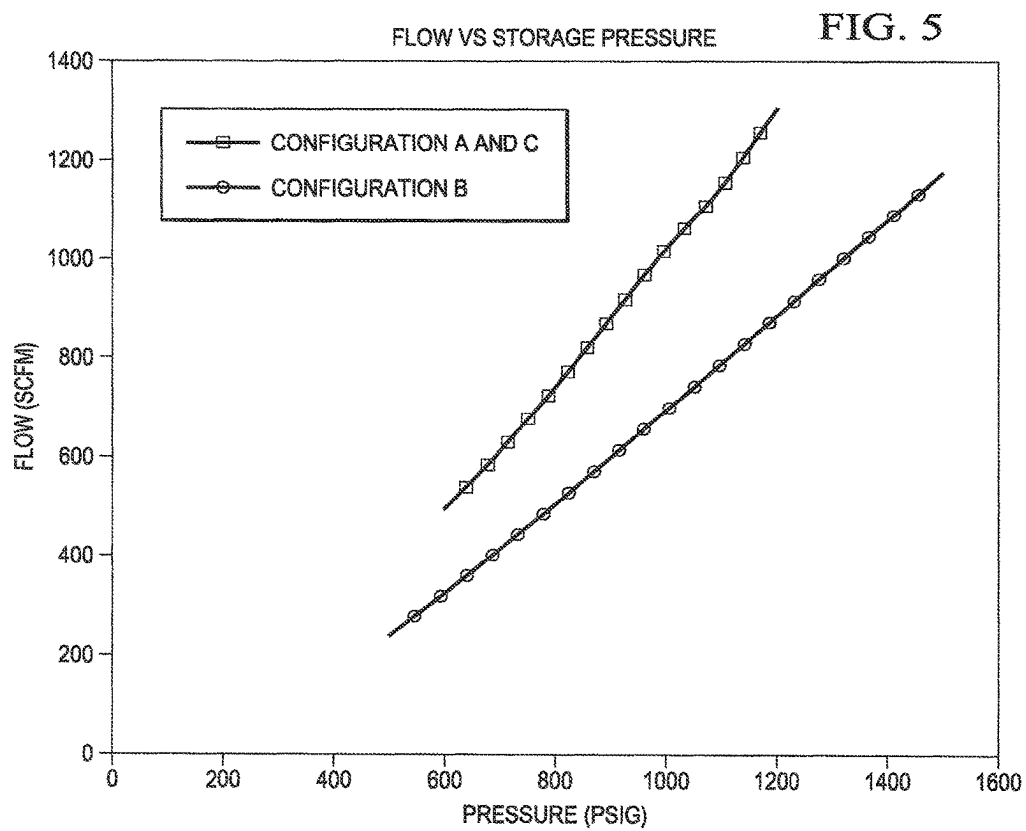


FIG. 2D





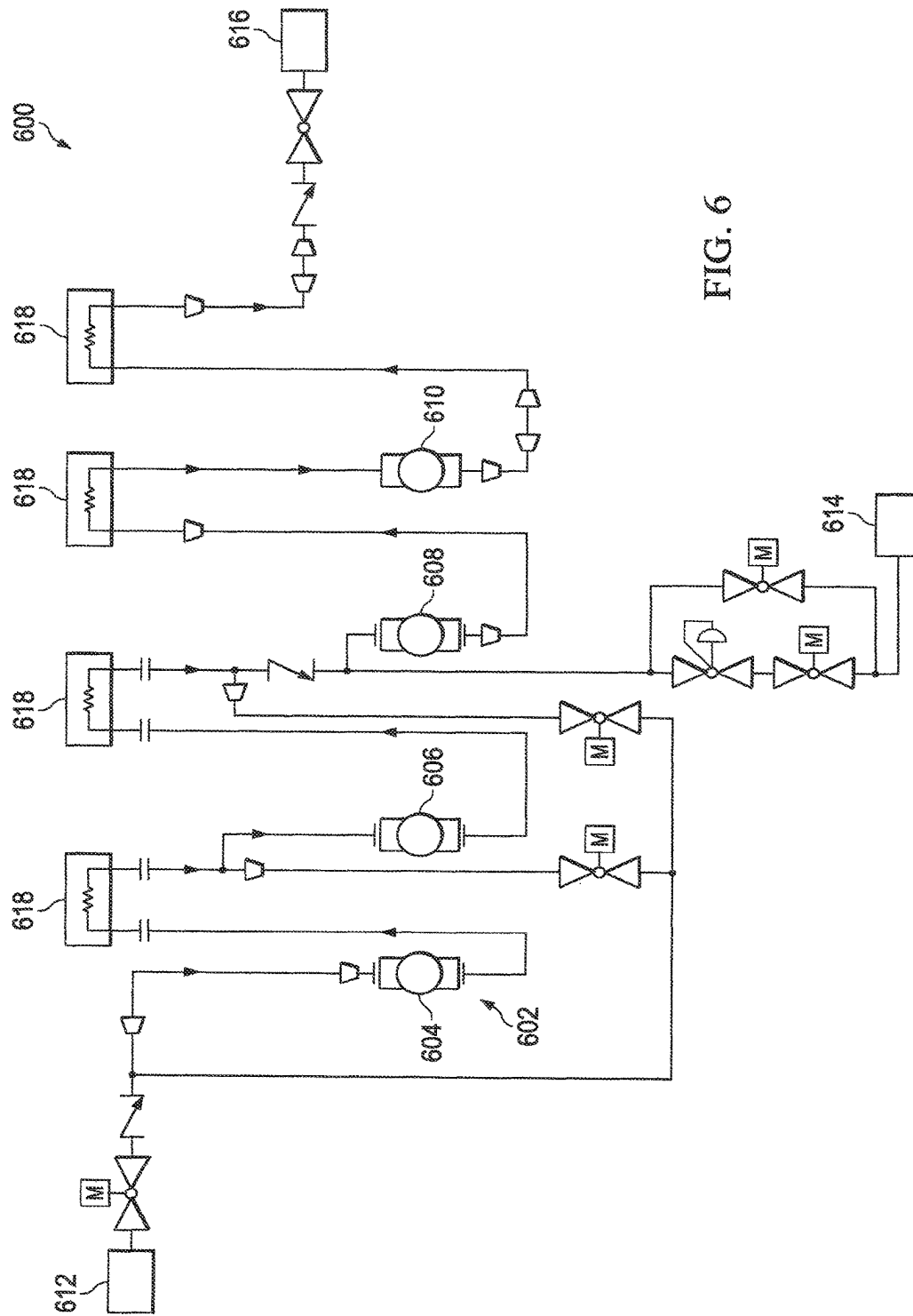
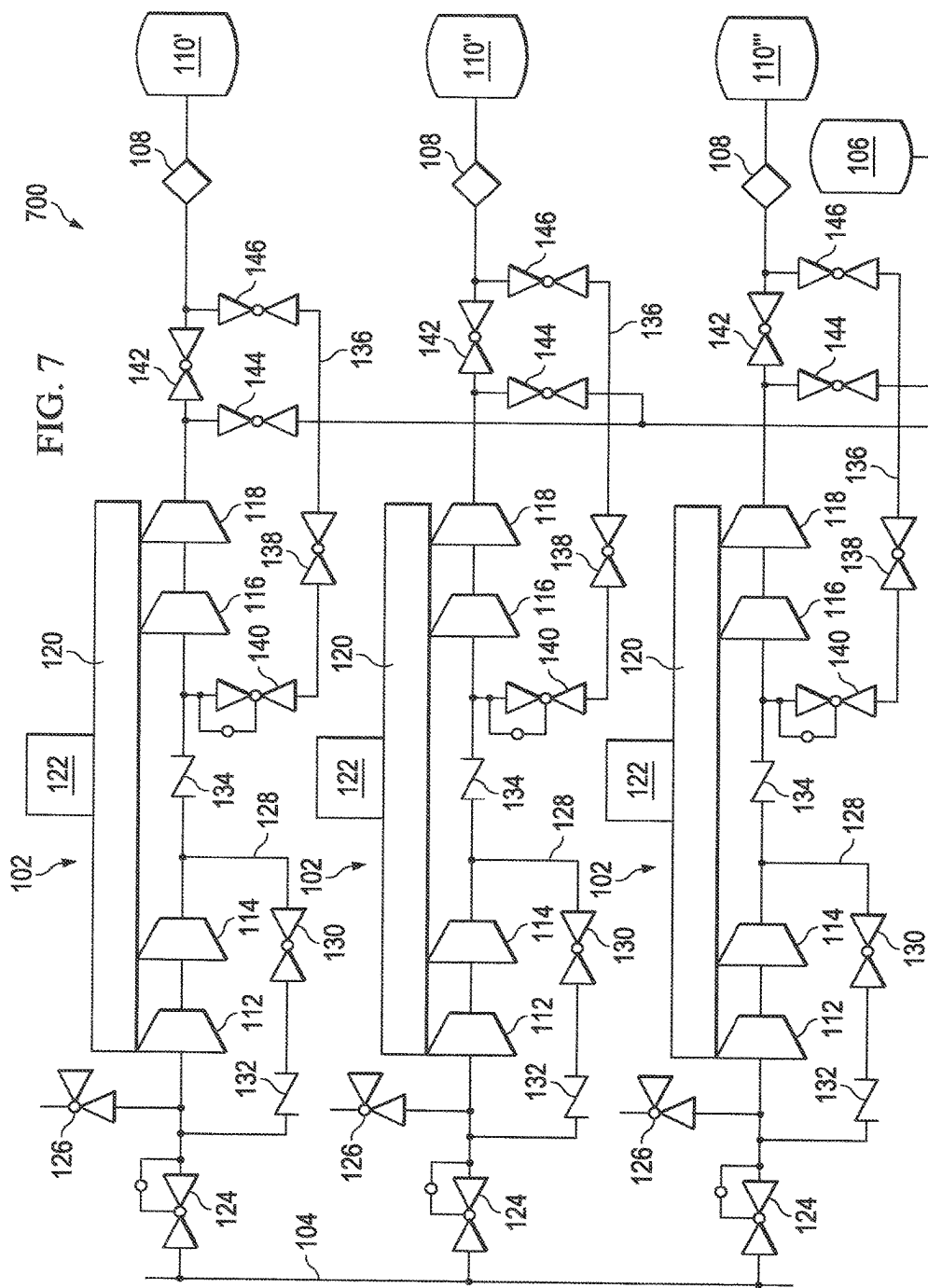


FIG. 6



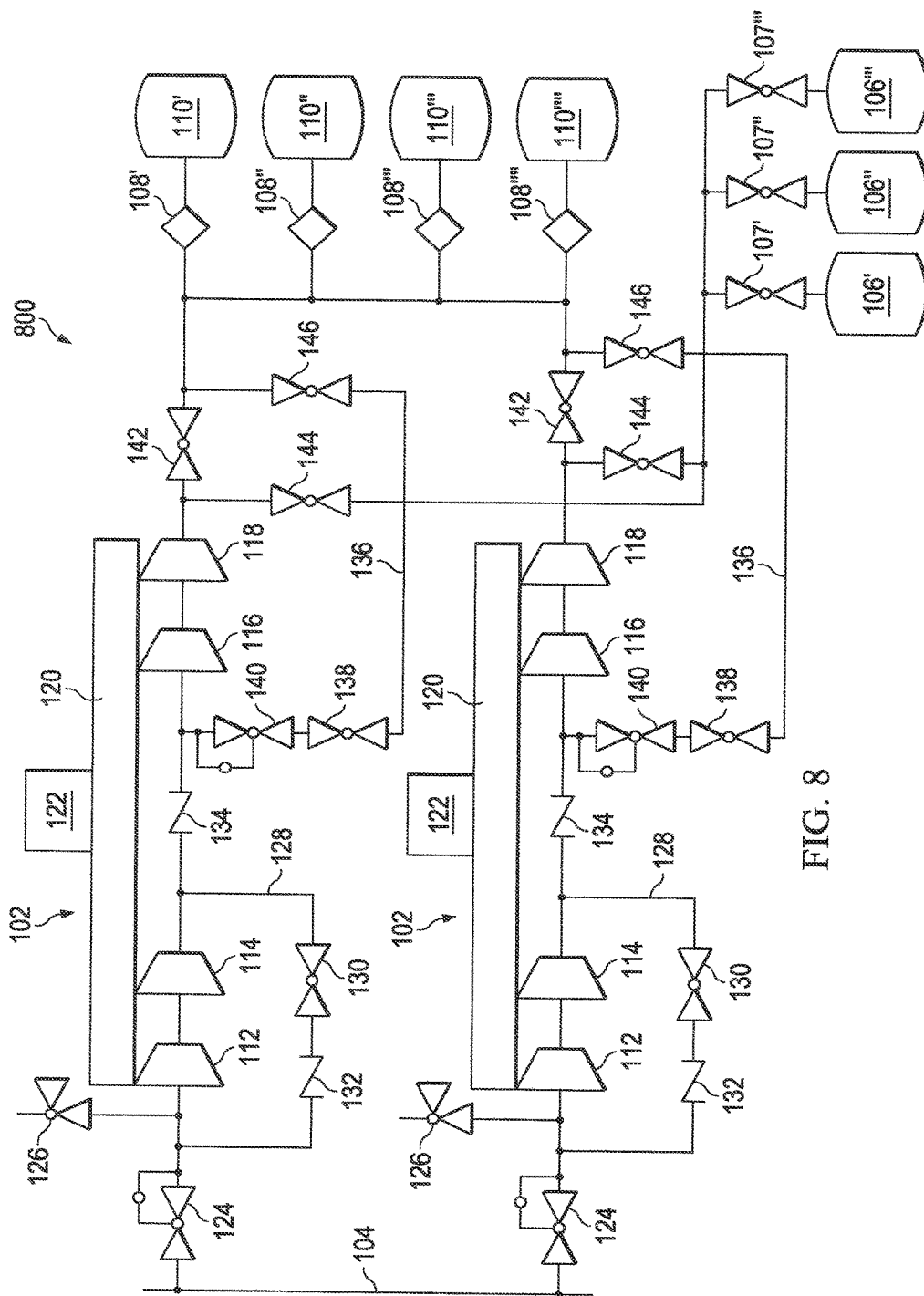


FIG. 8

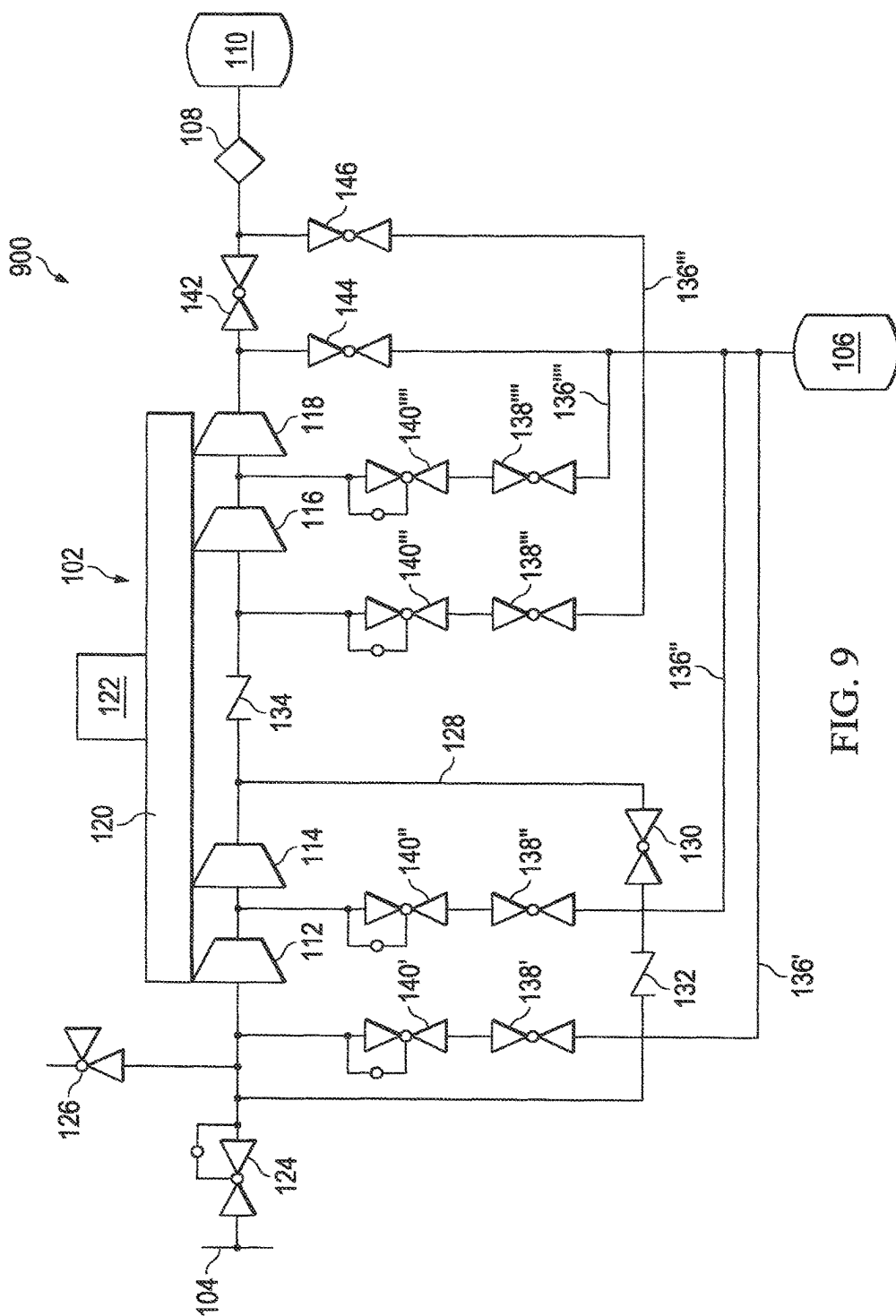
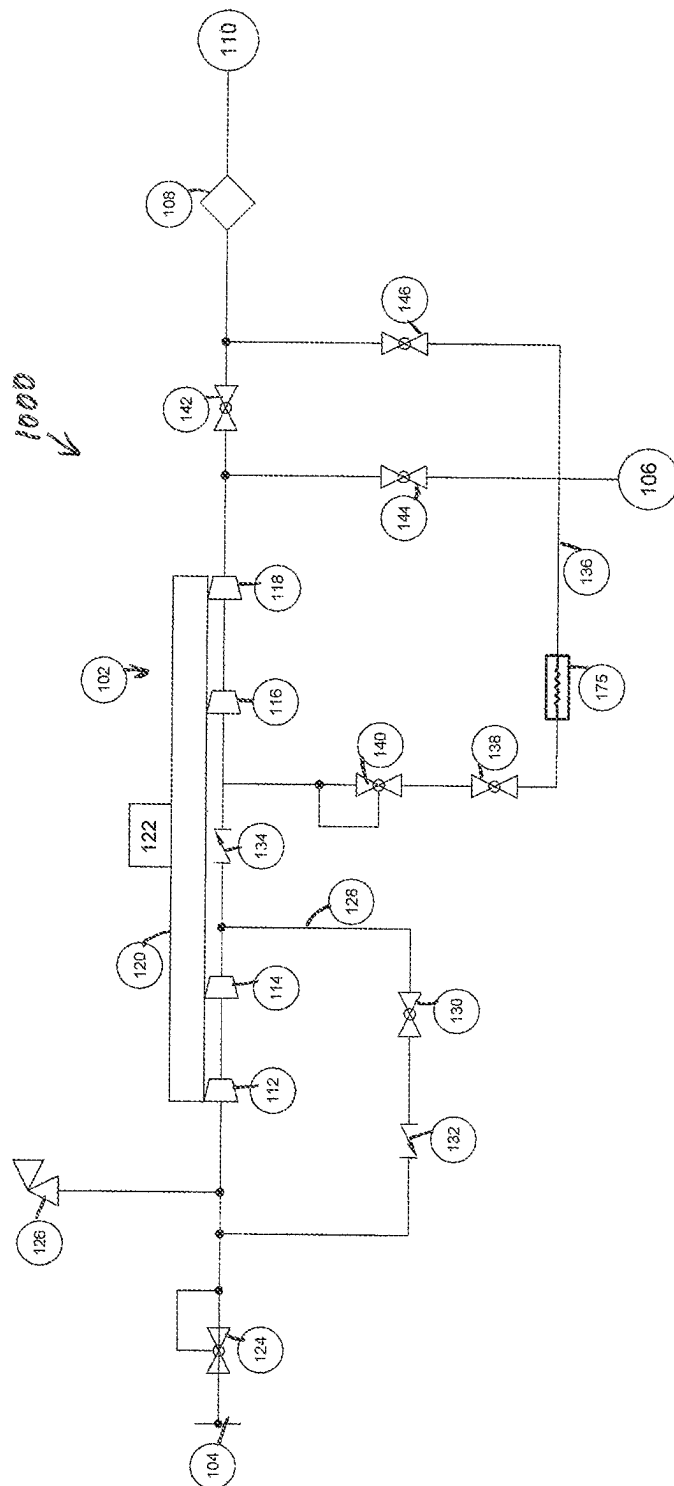
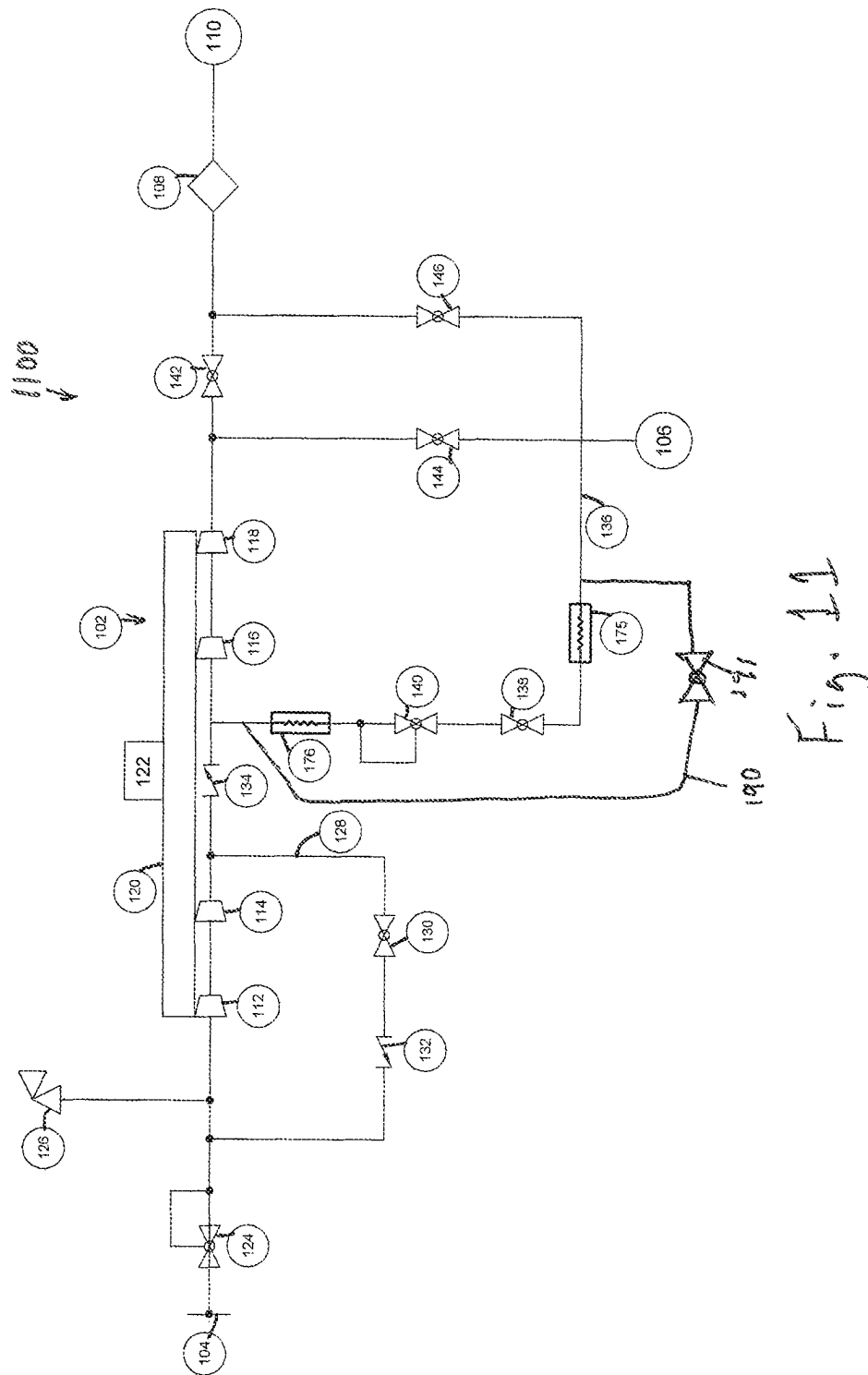


FIG. 9



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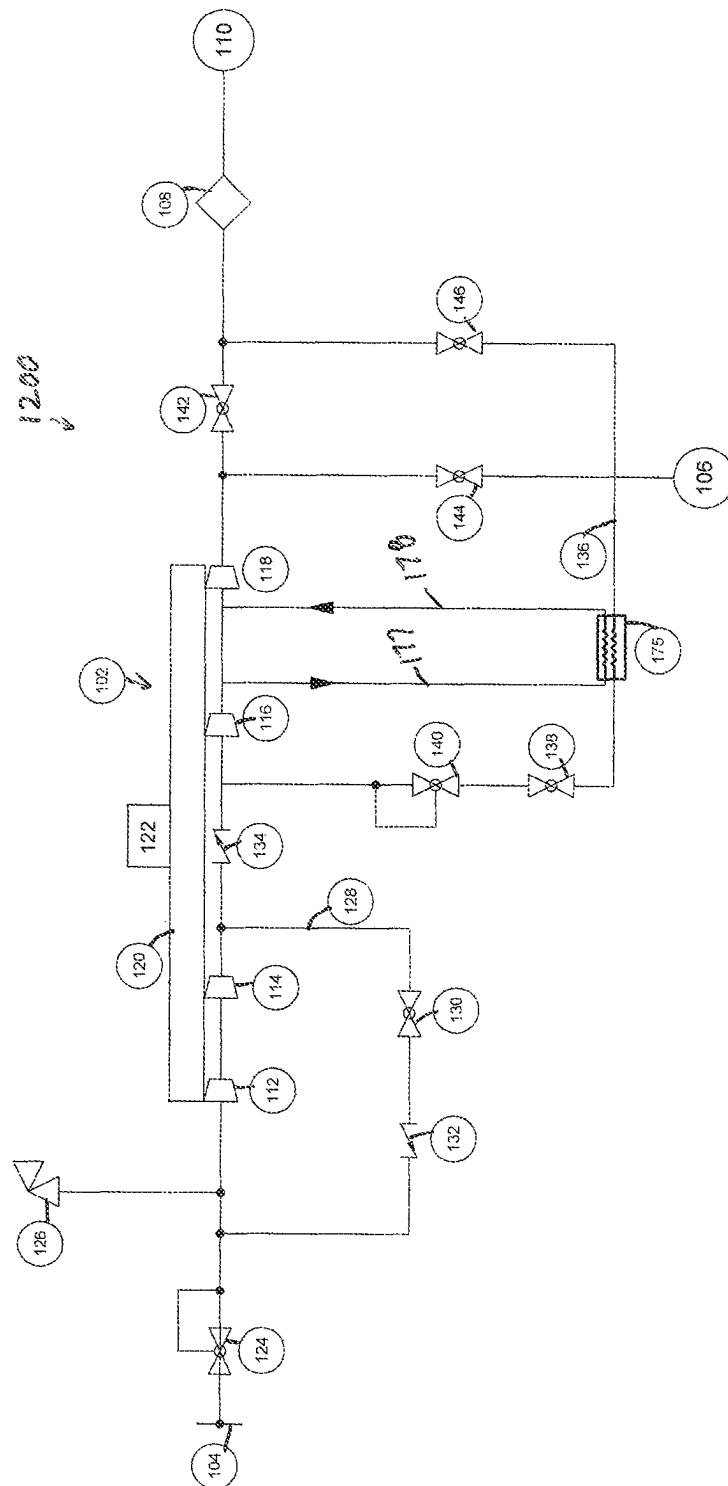


Fig. 12

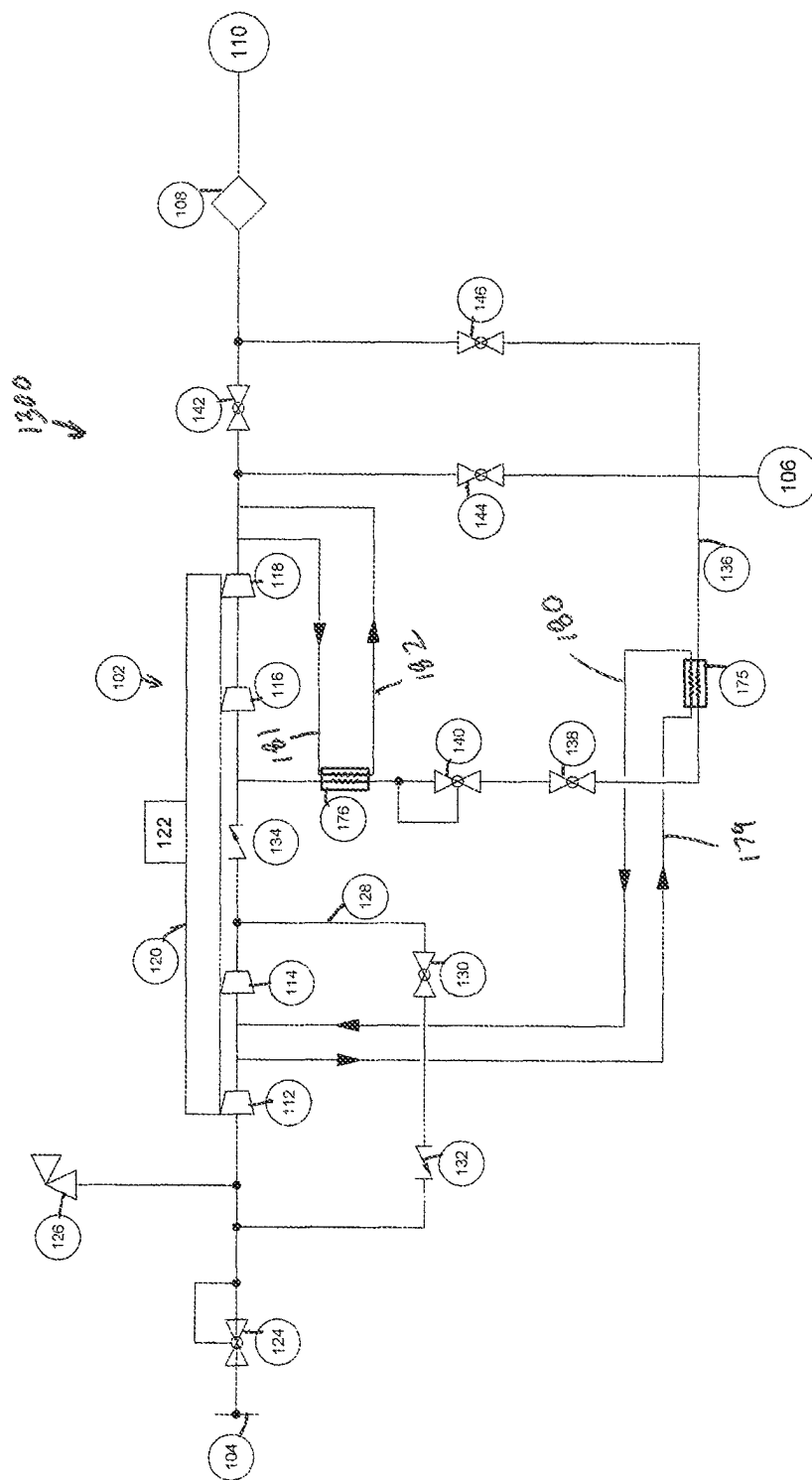


Fig. 13

CNG FUELING SYSTEM

BACKGROUND

Some compressed natural gas (CNG) fueling systems are configured for operation with relatively high natural gas source pressures. In some cases, CNG fueling systems comprise multiple compressors, multiple compressor crankshafts, and/or multiple compressor driver devices. In some cases, CNG fueling systems comprise multiple CNG storage tanks and/or are not capable of filling a fuel tank quickly.

SUMMARY

Some compressed natural gas (CNG) fueling systems are configured for operation with relatively high natural gas source pressures. In some cases, CNG fueling systems comprise multiple compressors, multiple compressor crankshafts, and/or multiple compressor driver devices. In some cases, CNG fueling systems comprise multiple CNG storage tanks and/or are not capable of filling a fuel tank quickly. In some embodiments of the disclosure, a compressed natural gas (CNG) fueling system is disclosed as comprising a single compressor, a storage tank configured to receive CNG from the compressor, and a CNG feedback to the compressor from the storage tank.

In other embodiments of the disclosure, a method of operating a compressed natural gas (CNG) fueling system is disclosed as comprising providing a single compressor, storing CNG compressed by the compressor, and further compressing the stored CNG using the compressor.

In yet other embodiments of the disclosure, a compressed natural gas (CNG) fueling system is disclosed as comprising a single separable reciprocating gas compressor comprising a plurality of compression stages, a storage tank configured to receive CNG from the compressor, and a feedback configured to provide CNG from the storage tank to at least one of the plurality of compression stages.

BRIEF DESCRIPTION OF THE DRAWINGS

For a more complete understanding of the present disclosure and the advantages thereof, reference is now made to the following brief description, taken in connection with the accompanying drawings and detailed description:

FIG. 1 is a schematic diagram of a CNG fueling system according to an embodiment of the disclosure.

FIG. 2A is a schematic diagram of the CNG fueling system of FIG. 1 showing a flowpath utilized while receiving natural gas from a source, compressing the natural gas, and storing the natural gas in a storage tank.

FIG. 2B is a schematic diagram of the CNG fueling system of FIG. 1 showing a flowpath utilized while transferring natural gas from a storage tank to a vehicle storage tank.

FIG. 2C is a schematic diagram of the CNG fueling system of FIG. 1 showing a flowpath utilized while providing natural gas from a storage tank to a compressor, compressing the natural gas, and transferring natural gas from the compressor to a vehicle storage tank.

FIG. 2D is a schematic diagram of the CNG fueling system of FIG. 1 showing a flowpath utilized while receiving natural gas from a natural gas source, compressing the natural gas, and providing the compressed natural gas to a vehicle storage tank.

FIG. 3 is a flowchart of a method of transferring fuel to a vehicle storage tank according to an embodiment of the disclosure.

FIG. 4 is a chart comparing gas flow versus natural gas source pressure for three different configurations of the CNG fueling system of FIG. 1.

FIG. 5 is a chart comparing gas flow versus storage tank pressure for the three different CNG fueling system configurations of FIG. 4.

FIG. 6 is a schematic diagram of a CNG fueling system according to another embodiment of the disclosure.

FIG. 7 is a schematic diagram of another CNG fueling system according to another embodiment of the disclosure.

FIG. 8 is a schematic diagram of another CNG fueling system according to another embodiment of the disclosure.

FIG. 9 is a schematic diagram of another CNG fueling system according to another embodiment of the disclosure.

FIG. 10 is a schematic diagram of another CNG fueling system according to another embodiment of the disclosure.

FIG. 11 is a schematic diagram of another CNG fueling system according to another embodiment of the disclosure.

FIG. 12 is a schematic diagram of another CNG fueling system according to another embodiment of the disclosure.

FIG. 13 is a schematic diagram of another CNG fueling system according to another embodiment of the disclosure.

DETAILED DESCRIPTION

Referring In some cases, it may be desirable to provide a CNG refueling system capable of speedily refueling a vehicle storage tank and/or any other suitable CNG related device without multiple compressors, multiple compressor drivers, and/or a high pressure natural gas source. In some embodiments, this disclosure provides a CNG refueling system comprising one compressor, one compressor driver, and/or a low pressure natural gas source. In some embodiments, the above-described CNG refueling system may be configured to feed CNG previously compressed by the compressor back into the same compressor and to transfer the recompressed CNG to a vehicle storage tank.

Referring now to FIG. 1, a schematic of a CNG fueling system 100 is shown according to an embodiment of the disclosure. The CNG fueling system 100 may generally comprise a compressor 102, a natural gas source 104, a storage tank 106, and a CNG dispenser 108. The CNG fueling system 100 may comprise a vehicle storage tank 110 and/or the CNG fueling system 100 may be configured to selectively transfer CNG to the vehicle storage tank 110. In this embodiment, the compressor 102 comprises four stages of compression represented by a first compression stage 112, a second compression stage 114, a third compression stage 116, and a fourth compression stage 118. In this embodiment, each of the compression stages 112, 114, 116, 118 may be powered by a power transfer device 120 that may comprise a single primary crankshaft that may drive pistons of the compression stages 112, 114, 116, 118 in a reciprocating manner within associated bores of the compression stages 112, 114, 116, 118. As such, the compressor 102 may comprise a separable reciprocating gas compressor. In some cases, the power transfer device 120 may be driven by a compressor driver 122, such as, but not limited to an electrical motor, a natural gas fueled engine, a turbine, an internal combustion engine, and/or any other device suitable for providing rotational power input and/or torque power input to the power transfer device 120. In alternative embodiments, the compressor 102 may comprise more or fewer compression stages, a rotary compressor, a scroll

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compressor, a pneumatic and/or hydraulically powered compressor, additional power transfer devices **120**, additional compressor drivers **122**, and/or any other suitable means for selectively compressing natural gas.

In this embodiment, the natural gas source **104** may comprise a relatively low source pressure of less than about 350 psig, between about 5 psig to about 330 psig, between about 70 psig to about 330 psig, between about 275 psig to about 325 psig, and/or about 300 psig. A source regulator valve **124** may be configured to limit a natural gas pressure provided to the compressor **102**, namely in this embodiment, the natural gas pressure provided to the first compression stage **112**. In some cases, the source regulator valve **124** may be adjusted to comprise a high pressure limit of less than about 350 psig, between about 5 psig to about 330 psig, between about 40 psig to about 330 psig, between about 275 psig to about 325 psig, and/or about 300 psig. In some cases, a pressure release valve **126** may be provided to selectively reduce pressure provided to the compressor **102**, namely in this embodiment, the natural gas pressure provided to the first compression stage **112**. In some cases, the pressure release valve **126** may be selected and/or adjusted to comprise a release pressure of less than about 350 psig, between about 5 psig to about 330 psig, between about 40 psig to about 330 psig, between about 275 psig to about 325 psig, and/or about 300 psig. In some embodiments, the pressure release valve **126** may be set to comprise a release pressure higher than the high pressure limit of the source regulator valve **124**. In some cases, the pressure release valve **126** may operate to release natural gas to atmosphere or storage.

In some embodiments, a stage bypass **128** may be provided in selective fluid communication with the natural gas source **104** and an output of the second compression stage **114**. The stage bypass **128** may comprise a stage bypass valve **130** operable to selectively open and close the stage bypass **128**. The stage bypass **128** may further comprise a bypass check valve **132**. Similarly, a second stage check valve **134** may be provided to prevent fluid from reaching the stage bypass **128** and/or the second compression stage **114** outlet from a storage feedback **136** that is in selective fluid communication with the storage tank **106** and the input to the third compression stage **116**. A feedback valve **138** may be provided to selectively open and close the storage feedback **136**. A feedback regulator valve **140** may be configured to comprise a high pressure limit equal to or less than a maximum pressure rating for an input of the third compression stage **116**.

FIG. 2A is a schematic diagram of the CNG fueling system **100** of FIG. 1 showing a flowpath **150** that may be selectively utilized to receive natural gas from the natural gas source **104**, compress natural gas using each of the compression stages **112**, **114**, **116**, **118** of the compressor **102**, and store the CNG in the storage tank **106**. FIG. 2B is a schematic diagram of the CNG fueling system **100** of FIG. 1 showing a flowpath **152** that may be selectively utilized to transfer CNG from the storage tank **106** to a vehicle storage tank **110** via the dispenser **108**. FIG. 2C is a schematic diagram of the CNG fueling system **100** of FIG. 1 showing a flowpath **154** that may be selectively utilized to provide CNG from the storage tank **106** to the compressor **102**, further compress the CNG, and transfer the further compressed CNG from the compressor **102** to the vehicle storage tank **110** via the dispenser **108**. In some embodiments, during operation of the compressor **102** as shown in FIG. 2C, the stage bypass valve **130** may be open to direct an output of the second compression stage **114** to an input of the first compression stage **112** thereby generally operating the

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first and second compression stages **112**, **114** in an unloaded state while operating the third and fourth stages **116**, **118** in a loaded state. FIG. 2D is a schematic diagram of the CNG fueling system **100** of FIG. 1 showing a flowpath **156** that may be selectively utilized to receiving natural gas from the natural gas source **104**, compress the natural gas, and providing the CNG to the vehicle storage tank **110** via the dispenser **108**.

In some embodiments, an output pressure of the first compression stage **112** may range from about 100 psig to about 1000 psig. In some embodiments, an output pressure of the second compression stage **114** may range from about 350 psig to about 1000 psig. In some embodiments, CNG may be supplied to the input of the third compression stage **116** at a pressure ranging from about 350 psig to about 1200 psig. In some embodiments, an output pressure of the third compression stage **116** may range from about 1000 psig to about 3000 psig. In some embodiments, CNG may be supplied to the input of the fourth compression stage **118** at a pressure ranging from about 1000 psig to about 3000 psig. In some embodiments, an output pressure of the fourth compression stage **118** may range from about 2000 psig to about 5000 psig.

In this embodiment, an output of the fourth compression stage **118** and the dispenser **108** may be selectively connected and/or disconnected from fluid communication with each other by a valve **142**. Further, the storage tank **106** may be selectively connected in fluid communication with an input of the valve **142** via a valve **144**. Similarly, the storage tank **106** may be selectively connected and/or disconnected in fluid communication with an output of the valve **142** via a valve **146**.

Referring now to FIG. 3, a method **300** of transferring fuel to a vehicle storage tank is shown according to an embodiment of the disclosure. The method **300** may begin at block **302** by providing a single compressor, such as a compressor **102**. In some embodiments, a grouping of gas compression components may be a single compressor if at least one of (1) the gas compression components (i.e. pistons and/or the like) are driven by a single and/or shared rotating input, such as, but not limited to, a crankshaft of a power transfer device **120** and (2) the gas compression components and/or the power transfer devices are driven by a single and/or shared compressor driver, such as, but not limited to, a single compressor driver **122** (i.e. electric motor). The method **300** may continue at block **304** by storing CNG compressed by the single compressor. The method **300** may continue at block **306** by further compressing the stored CNG using the single compressor. The method **300** may continue at block **308** by transferring the further compressed CNG to a vehicle storage tank **110**.

In some cases, a CNG fueling system **100** may operate as shown in FIG. 2A until the storage tank **106** has reached a maximum capacity at a selected CNG pressure, in some cases, about 4500 psig to about 5000 psig. With the storage tank **106** full, the compressor **102** may turn off. Next, CNG may be provided to a vehicle storage tank **110** from the storage tank **106** as shown in FIG. 2B until the storage tank **106** and the vehicle storage tank **110** either equalize or until a mass flow rate or transfer rate of CNG falls below a predetermined threshold value. In some embodiments, when the above-described equalization or predetermined threshold value is reached, or when a lower predetermined pressure of the storage tank **106** is reached, the CNG fueling system **100** may operate as shown in FIG. 2C to direct CNG from the storage tank **106** to at least one of the compression stages **112**, **114**, **116**, **118** of the compressor **102** and transfer the

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further compressed CNG from the running compressor **102** to the vehicle storage tank **110**. In some embodiments, after another predetermined lower pressure threshold of the storage tank **106** is reached, the system may continue to provide CNG to the vehicle storage tank **110** by operating as shown in FIG. 2D until the vehicle storage tank **110** is full as indicated by pressure, weight, change in mass flow rate, and/or any other suitable determinative factor. In the manner described above, a single compressor may be utilized to quickly fill a vehicle storage tank with CNG even when the natural gas source is provided at a relatively low pressure.

Referring now to FIG. 4, a chart comparing gas flow versus natural gas source pressure for three different configurations of the CNG fueling system of FIG. 1. FIG. 5 is a chart comparing gas flow versus storage tank pressure for the three different CNG fueling systems substantially similar to the CNG fueling system **100** configurations of FIG. 1. In each of FIGS. 4 and 5, reference is made to configurations A, B, and C. Each of configurations A, B, and C illustrate operation of CNG fueling systems **100** with an electric motor compressor drive **122** driving a single and/or shared crankshaft of a power transfer device **120** at 1800 rpm with a 3 inch stroke length. The differences between configurations A, B, and C are the compressor driver **122** size (horsepower), the number of compression stages, and the cylinder bore diameter of the compressions stages of the separable CNG compressor **102**. Configuration A comprises a 250 HP electric motor, a 1st stage 7¼" bore, a 2nd stage 4⅝" bore, a 3rd stage 3⅜" bore, and a 4th stage 1¾" bore, where CNG is fed back to the 3rd and 4th stage during operation substantially similar to that shown in FIG. 2C. Configuration B comprises a 125 HP electric motor, a 1st stage 8" bore, a 2nd stage 4⅝" bore, a 3rd stage 3" bore, and a 4th stage 1½" bore, where CNG is fed back to the 3rd and 4th stage during operation substantially similar to that shown in FIG. 2C. Configuration C comprises a 250 HP electric motor, a 1st stage 4⅝" bore, a 2nd stage 3⅜" bore, and a 3rd stage 1¾" bore, where CNG is fed back to the 2nd and 3rd stage during operation substantially similar to that shown in FIG. 2C.

FIG. 6 is a schematic diagram of a CNG fueling system **600** according to another embodiment of the disclosure. CNG fueling system **600** is substantially similar to CNG fueling system **100**. CNG fueling system **600** comprises a single compressor **602** comprising a first compression stage **604**, a second compression stage **606**, a third compression stage **608**, and a fourth compression stage **610**. Also like CNG fueling system **100**, CNG fueling system **600** is configured to receive natural gas from a relatively low pressure natural gas source **612** having a pressure of about 330 psig or less. The CNG fueling system **600** may be configured to compress natural gas and deliver the CNG to each of a storage tank **614** and a vehicle storage tank **616**. The CNG fueling system **600** may be operated substantially in accordance with the method **300** to quickly fuel a vehicle storage tank **616**. CNG fueling system **600** further comprises a plurality of heat exchangers **618** through which CNG may be passed to manage a temperature of the CNG as it moves relative to the compression stages **604**, **606**, **608**, **610**.

Referring now to FIG. 7, a schematic diagram of a CNG fueling system **700** according to another embodiment of the disclosure is shown. CNG fueling system **700** comprises a plurality of compressors **102** that are substantially similar to compressors **102** of CNG fueling system **100**. Each compressor **102** may be provided natural gas from the natural gas source **104**. In this embodiment, multiple vehicle storage tanks **110'**, **110"**, **110'''** may be provided CNG by CNG

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fueling system **700** substantially independently of each other. In this embodiment, each compressor **102** may be configured to deliver CNG to a shared and/or same storage tank **106**. In alternative embodiments, a CNG storage selection header may be provided that comprises any necessary pipes, valves, and/or control systems useful in selectively directing a CNG output from any combination of compressors **102** to storage tank **106** and/or to any combination of a plurality of storage tanks **106**. In alternative embodiments, a dispenser selection header may be provided that comprises any necessary pipes, valves, and/or control systems useful in selectively directing a CNG output from any combination of compressors **102** to any combination of the plurality of dispensers **108**.

Referring now to FIG. 8, a schematic diagram of a CNG fueling system **800** according to another embodiment of the disclosure is shown. CNG fueling system **800** comprises a plurality of compressors **102** that are substantially similar to compressors **102** of CNG fueling system **100**. Each compressor **102** may be provided natural gas from the natural gas source **104**. In this embodiment, multiple vehicle storage tanks **110'**, **110"**, **110'''**, **110''''** may be provided CNG by CNG fueling system **800** substantially independently of each other. In this embodiment, each compressor **102** may be configured to deliver CNG to a shared and/or same storage tank **106**. In this embodiment, each storage tank **106'**, **106"**, **106'''** is provided with a tank valve **107'**, **107"**, **107'''**, respectively, to allow any combination of selections of storage tanks **106'**, **106"**, **106'''** to receive and/or provide CNG. In alternative embodiments, a CNG storage selection header may be provided that comprises any necessary pipes, valves, and/or control systems useful in selectively directing a CNG output from any combination of compressors **102** to storage tanks **106'**, **106"**, **106'''**. In alternative embodiments, a dispenser selection header may be provided that comprises any necessary pipes, valves, and/or control systems useful in selectively directing a CNG output from any combination of compressors **102** to any combination of the plurality of dispensers **108'**, **108"**, **108'''**, **108''''**.

Referring now to FIG. 9, a schematic diagram of a CNG fueling system **900** according to another embodiment of the disclosure is shown. CNG fueling system **900** is substantially similar to CNG fueling system **100**. However, CNG fueling system **900** comprises a plurality of storage feedbacks **136'**, **136"**, **136'''**, **136''''**. In this embodiment, each storage feedback **136'**, **136"**, **136'''**, **136''''** is associated with their own dedicated feedback valves **138** (namely feedback valves **138'**, **138"**, **138'''**, **138''''**, respectively) and feedback regulator valves **140** (namely feedback regulator valves **140'**, **140"**, **140'''**, **140''''**, respectively). In some embodiments, the CNG fueling system **900** may control feedback valves **138'**, **138"**, **138'''**, **138''''** to selectively feed CNG back from storage tank **106** to any combination of compression stages **112**, **114**, **116**, **118**, sequentially and/or simultaneously. In some embodiments, additional CNG storage tanks may be provided and selectively filled to comprise CNG at pressures higher or lower than storage tank **106**. In alternative embodiments, a feedback header may be provided that comprises any necessary pipes, valves, and/or control systems useful in selectively directing a CNG output from any combination of storage tanks **106** to any combination of the plurality of compression stages **112**, **114**, **116**, **118** via the storage feedbacks **136'**, **136"**, **136'''**, **136''''**.

In some embodiments, the CNG fueling system **900** may be operated to feed CNG back from storage tank **106** to fourth compression stage **118** via storage feedback **136''''** until the pressure of the CNG supplied by the storage tank

106 is reduced to a first predetermined threshold pressure. In some embodiments, the first predetermined threshold pressure may be associated with a lower end of a desirable input pressure range of the fourth compression stage **118**. Once the first predetermined threshold pressure is reached, the CNG fueling system **900** may be operated to discontinue feeding CNG back from storage tank **106** to fourth compression stage **118**.

In some embodiments, the CNG fueling system **900** may be operated to feed CNG back from storage tank **106** to third compression stage **116** via storage feedback **136'** until the pressure of the CNG supplied by the storage tank **106** is reduced to a second predetermined threshold pressure. In some embodiments, the second predetermined threshold pressure may be associated with a lower end of a desirable input pressure range of the third compression stage **116**. Once the second predetermined threshold pressure is reached, the CNG fueling system **900** may be operated to discontinue feeding CNG back from storage tank **106** to third compression stage **116**.

In some embodiments, the CNG fueling system **900** may be operated to feed CNG back from storage tank **106** to second compression stage **114** via storage feedback **136''** until the pressure of the CNG supplied by the storage tank **106** is reduced to a third predetermined threshold pressure. In some embodiments, the third predetermined threshold pressure may be associated with a lower end of a desirable input pressure range of the second compression stage **114**. Once the third predetermined threshold pressure is reached, the CNG fueling system **900** may be operated to discontinue feeding CNG back from storage tank **106** to second compression stage **114**.

In some embodiments, the CNG fueling system **900** may be operated to feed CNG back from storage tank **106** to first compression stage **112** via storage feedback **136'''** until the pressure of the CNG supplied by the storage tank **106** is reduced to a fourth predetermined threshold pressure. In some embodiments, the fourth predetermined threshold pressure may be associated with a lower end of a desirable input pressure range of the first compression stage **112**. Once the fourth predetermined threshold pressure is reached, the CNG fueling system **900** may be operated to discontinue feeding CNG back from storage tank **106** to first compression stage **112**. In some embodiments, once the CNG fueling system **900** discontinues feeding CNG back from storage tank **106** to first compression stage **112**, the CNG fueling system **900** may begin operation substantially similar to that shown in FIG. 2D to complete fueling a vehicle storage tank **110**.

While the CNG fueling systems disclosed above are described with specificity, it will be appreciated that alternative embodiments of CNG fueling systems are contemplated that comprise any necessary header and/or fluid distribution systems useful in selectively connecting any of the component parts of the CNG fueling systems in any combination. For example, alternative embodiments may comprise headers, valves, pipes, control systems, and/or any other suitable device for selectively connecting one or more storage tanks to one or more compressors, compression stages, dispensers, vehicle storage tanks, alternative natural gas supplies, and/or any other suitable interface. Similarly, alternative embodiments may comprise headers, valves, pipes, control systems, and/or any other suitable device for selectively connecting one or more compressors and/or compression stages to one or more compressors, compression stages, dispensers, vehicle storage tanks, alternative natural gas supplies, and/or any other suitable interface.

Similarly, alternative embodiments may comprise headers, valves, pipes, control systems, and/or any other suitable device for selectively connecting one or more dispensers to one or more compressors, compression stages, dispensers, vehicle storage tanks, alternative natural gas supplies, and/or any other suitable interface. Similarly, alternative embodiments may comprise headers, valves, pipes, control systems, and/or any other suitable device for selectively connecting one or more vehicle storage tanks to one or more compressors, compression stages, dispensers, alternative natural gas supplies, and/or any other suitable interface. In some embodiments, the above-described systems and methods may comprise systems and/or methods for being implemented in an automated, semi-automated, programmed, electronically controlled, manual, and/or computer controlled nature. In some embodiments, the above-described systems and methods may be remotely controlled and/or robotically assisted.

In some cases, CNG stored in a storage tank, such as storage tank **106**, may experience a reduction in temperature. One reason CNG stored in a storage tank may be cooled is because the storage tank **106** may be located above ground and exposed to cold ambient temperatures. In some geographic locations, the ambient temperatures may be as low as -20 degrees Fahrenheit or lower. Secondly, the stored CNG may experience a temperature decrease because of the Joule-Thompson effect according to which gasses are cooled as they expand. Accordingly, as CNG is removed from the storage tank, the removed CNG expands and cools and also causes some cooling of CNG remaining in the storage tank. In some embodiments, as the compressor pulls gas from storage, the storage tank may reduce from about 4000 psig to about 1000 psig. This 3000 psig decrease will cause the gas left in storage to decrease in temperature. The storage vessel may eventually warm the CNG that remains in storage, but the gas that is provided to the compressor may remain relatively cooler. Without means to prevent otherwise, the temperature of the CNG provided to the compressor may be undesirably cool, and that temperature depends how fast the gas is removed from the storage tank. Feeding cold gas to the compressor can be problematic. In some cases, cold gas can overload a driver of the compressor since colder gas is denser and more power is required to compress it. In other cases, the cold gas may shift a load on a piston rod of the compressor when gas flow is increased, thereby causing problems with the piston rod. Still further, the cool gas may reduce system equipment temperatures to near or below minimum design metal temperatures (MDMT) which can cause metal to become brittle and increase a risk of fracture. Accordingly, the embodiments of FIGS. 10-13 are disclosed which provide for warming the CNG temperature before providing it to the compressor from the storage tank.

Referring now to FIG. 10, a schematic of a CNG fueling system **1000** is shown according to an embodiment of the disclosure. The CNG fueling system **1000** is substantially similar to the CNG fueling system **100** but for the addition of the heat exchanger **175** disposed along the storage feedback **136**. In this embodiment, the heat exchanger **175** is disposed between the storage tank **106** and the feedback valve **138**. The heat exchanger **175** can comprise any suitable type of heat exchanger that can warm the CNG flowing from the storage tank **106** to the feedback valve **138**. In some cases, the heat exchanger may comprise an electrical heating element, a furnace, a fan, and/or any other suitable system or device. In some embodiments, the heat exchanger **175** can be operated to provide varying degrees of

heat as a function of the ambient temperature, CNG temperature, and/or a desired temperature of CNG being delivered to the compressor 102.

Referring now to FIG. 11, a schematic of a CNG fueling system 1100 is shown according to an embodiment of the disclosure. The CNG fueling system 1100 is substantially similar to the CNG fueling system 1000 but for the addition of the heat exchanger 176 also disposed along the storage feedback 136. In this embodiment, the heat exchanger 176 is disposed between the feedback regulator valve 140 and the compressor 102. More specifically, the heat exchanger 176 is disposed between feedback regulator valve 140 and the third compression stage 116. Like heat exchanger 175, heat exchanger 176 may comprise an electrical heating element, a furnace, a fan, and/or any other suitable system or device.

Referring now to FIG. 12, a schematic of a CNG fueling system 1200 is shown according to an embodiment of the disclosure. The CNG fueling system 1200 is substantially similar to the CNG fueling system 1000, but with the additional of a heater input line 177 and a heater output line 178. In this embodiment, the heater input line 177 provides hot gas from an output of the third compression stage 116 to the heat exchanger 175 and the heater output line 178 returns hot gas (albeit potentially slightly cooler than when first supplied to the heat exchanger 175) to the compressor 102 and to an input of the fourth compression stage 118. In some embodiments, the heat exchanger 175 may comprise a pipe-in-pipe type heat exchanger. In some cases, during operation of the heat exchanger 175 to warm CNG as it is provided to the third compression stage, the first compression stage 112 and the second compression stage 114 may be inactive or underutilized.

Referring now to FIG. 13, a schematic of a CNG fueling system 1300 is shown according to an embodiment of the disclosure. The CNG fueling system 1300 is substantially similar to the CNG fueling system 1100, but with the additional of a heater input lines 179, 181 and heater output lines 180, 182. In this embodiment, the heater input line 179 provides hot gas from an output of the first compression stage 112 to the heat exchanger 175 and the heater output line 180 returns hot gas (albeit potentially slightly cooler than when first supplied to the heat exchanger 175) to the compressor 102 and to an input of the second compression stage 114. In this embodiment, the heater input line 181 provides hot gas from an output of the fourth compression stage 118 to the heat exchanger 176 and the heater output line 182 returns hot gas (albeit potentially slightly cooler than when first supplied to the heat exchanger 175) to the output of the fourth compression stage 118. In some embodiments, the heat exchangers 175, 176 may comprise a pipe-in-pipe type heat exchangers, but any other suitable heat exchanger type is contemplated. In the extreme case where CNG pressure of the storage tank 106 drops from 4000 psig to about 600 psig, a 100 degree Fahrenheit temperature drop may occur and if the ambient temperature is below 80 degrees Fahrenheit, a dangerously low CNG and system temperature of below -20 degrees Fahrenheit may occur which is lower than the MDMT for most carbon steels. Accordingly, heat exchanger 175 is utilized to heat the gas up before further dropping pressure and temperature at feedback regulator valve 140. Thereafter, heat exchanger 176 can further heat the CNG.

Referring back to FIG. 11, in some embodiments, a cool gas bypass 190 may be provided that selectively receives cool CNG from upstream relative to the heat exchanger 175 and provides the cool gas downstream relative to the heat

exchanger 176. In some embodiments, a mixer valve 191 can be modulated to selected positions to provide a desired amount of cool CNG to mix with the warmed CNG exiting the heat exchanger 176. In other words, by providing a source of cool gas and a means for throttling the amount of cool gas to be mixed with warmer gas, CNG of a desired temperature can be provided to the compressor 102. Accordingly, this disclosure contemplates utilizing heat generated by the compressor 102 to warm CNG exiting the storage tank 106 and further contemplates fine tuning and/or otherwise adjusting a temperature of CNG to be provided to the compressor by mixing the warmed CNG with relatively cooler gas from the storage tank 106. Furthermore, by utilizing a feedback regulator valve 140, the allowable storage pressure of the storage tank 106 can be much higher than the maximum desired input pressure of the input of the third compression stage 116, thereby allowing use of a standard four stage compressor rather than requiring higher rated compression stages capable of handling the maximum storage pressure of the storage tank 106.

In some embodiments, a CNG system can be transitioned from operating only third compression stage 116 and fourth compression stage 118 (while drawing CNG from storage tank 106). In some cases, an input pressure to the third compression stage 116 can be higher while drawing CNG from storage tank 106 as compared to when drawing from the second stage 114 during four stage operation. To transition from the above-described two stage operation to four stage operation, the CNG supply from the storage tank 106 can be shut off (such as by closing feedback valve 138). As the pressure supplied to third compression stage 116 drops, it will approach a pressure that is typical for four stage operation. Once the pressure is substantially the same as four stage operation, the first compression stage 112 and the second compression stage 114 can be activated, thereby initiating four stage operation from a two stage operation in a very smooth manner.

At least one embodiment is disclosed and variations, combinations, and/or modifications of the embodiment(s) and/or features of the embodiment(s) made by a person having ordinary skill in the art are within the scope of the disclosure. Alternative embodiments that result from combining, integrating, and/or omitting features of the embodiment(s) are also within the scope of the disclosure. Where numerical ranges or limitations are expressly stated, such express ranges or limitations should be understood to include iterative ranges or limitations of like magnitude falling within the expressly stated ranges or limitations (e.g., from about 1 to about 10 includes, 2, 3, 4, etc.; greater than 0.10 includes 0.11, 0.12, 0.13, etc.). For example, whenever a numerical range with a lower limit, R_l , and an upper limit, R_u , is disclosed, any number falling within the range is specifically disclosed. In particular, the following numbers within the range are specifically disclosed: $R = R_l + k \cdot (R_u - R_l)$, wherein k is a variable ranging from 1 percent to 100 percent with a 1 percent increment, i.e., k is 1 percent, 2 percent, 3 percent, 4 percent, 5 percent, . . . 50 percent, 51 percent, 52 percent, . . . , 95 percent, 96 percent, 97 percent, 98 percent, 99 percent, or 100 percent. Moreover, any numerical range defined by two R numbers as defined in the above is also specifically disclosed. Use of the term "optionally" with respect to any element of a claim means that the element is required, or alternatively, the element is not required, both alternatives being within the scope of the claim. Use of broader terms such as comprises, includes, and having should be understood to provide support for narrower terms such as consisting of, consisting essentially of, and

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comprised substantially of. Accordingly, the scope of protection is not limited by the description set out above but is defined by the claims that follow, that scope including all equivalents of the subject matter of the claims. Each and every claim is incorporated as further disclosure into the specification and the claims are embodiment(s) of the present invention.

What is claimed is:

1. A compressed natural gas (CNG) fueling system, comprising:

a single compressor comprising a first compression stage and a subsequent compression stage, wherein the first compression stage feeds the subsequent compression stage when filling a storage tank;

the storage tank being configured to receive CNG from at least one of the first compression stage and the subsequent compression stage of the compressor when filling the storage tank;

a CNG feedback to the subsequent compression stage of the compressor from the storage tank, the CNG being introduced back into the compressor at a location downstream relative to an output of the first compression stage; and

a first heat exchanger associated with the CNG feedback.

2. The CNG fueling system of claim 1, wherein the first heat exchanger receives heated CNG from the compressor.

3. The CNG fueling system of claim 2, further comprising:

a feedback regulator valve disposed between the first heat exchanger and the compressor.

4. The CNG fueling system of claim 1, further comprising:

a second heat exchanger associated with the CNG feedback.

5. The CNG fueling system of claim 4, wherein at least one of the first heat exchanger and the second heat exchanger receive heated CNG from the compressor.

6. The CNG fueling system of claim 4, wherein each of the first heat exchanger and the second heat exchanger received heated CNG from the compressor.

7. The CNG fueling system of claim 4, further comprising a feedback regulator valve disposed between the first heat exchanger and the second heat exchanger.

8. A method of operating a compressed natural gas (CNG) fueling system, comprising:

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providing a single compressor comprising a first compression stage and a subsequent compression stage, wherein the first compression stage feeds the subsequent compression stage when filling a storage tank; compressing CNG using at least one of the first compression stage and the subsequent compression stage when filling the storage tank;

storing CNG compressed by the at least one of the first compression stage and the subsequent compression stage of the compressor in the storage tank;

further compressing the stored CNG using the compressor by feeding the stored CNG back to the subsequent compression stage of the compressor that compressed the CNG prior to storing the CNG in the storage tank, the CNG being introduced back into the compressor at a location downstream relative to an output of the first compression stage; and

providing a first heat exchanger and heating the CNG from the storage tank prior to feeding the CNG back to the subsequent compression stage.

9. The method of claim 8, wherein the first heat exchanger uses heat from the compressor to heat the CNG from the storage tank.

10. The method of claim 8, further comprising:

providing a feedback regulator valve between the first heat exchanger and the compressor.

11. The method of claim 10, operating the feedback regulator valve to output CNG at a pressure lower than a storage tank pressure.

12. The method of claim 8, further comprising:

providing a second heat exchanger between the compressor and the first heat exchanger.

13. The method of claim 12, further comprising:

providing a feedback regulator valve between the first heat exchanger and the second heat exchanger.

14. The method of claim 13, wherein the first heat exchanger receives heated CNG from an output of the first compression stage.

15. The method of claim 14, further comprising:

providing a cool CNG bypass connected between the storage tank and the first heat exchanger and connected between the compressor and the second heat exchanger.

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